



Tube Rupture Scenario E-3003



1. Heat Exchanger Data Input

High pressure side	Syngas
Low pressure side	CW
Design Pressure of high-pressure side	99 barg
Design Pressure of low-pressure side	7.5 barg
Operating Pressure	83.7 barg
M	10.07
Cp/Cv	1.37
Z	1
Relieving Temperature	41.8
Tube OD	25.4
Tube Thk.	1.65

2. Check if a PSV is needed

In order to perform this step, do the calculation below:

multiply design pressure of high-pressure side by 10/13:

$$99 * 10/13 = 76.15 \text{ barg}$$

So, design pressure of low-pressure side should be at least 76.15 barg in order not to need a PSV. Here it is 7.5 bars, thereby requiring a PSV.



3. Use the formula below to calculate Relief Load

<p>K_G : 2.93 (Metric), 385 (USC)</p> <p>K_L : 1.77 (Metric), 2645 (USC)</p>	<p>Vapors</p> <p>Liquids</p>	$W_G = K_G d^2 P_1 \sqrt{\frac{M}{zT}}$ $W_L = K_L d^2 \sqrt{\rho_L (P_1 - P_2)}$
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- W_G : gas flow through tube break, kg/hr or lb/hr
- W_L : liquid flow through tube break, kg/hr or lb/hr
- d : tube inside diameter, mm or inch
- $P_1(*)$: HP side normal pressure, bara or psia
(alternatively the HP side design pressure may be considered for P_1 , as required by some clients).
- $P_2(*)$: relieving pressure of the low pressure side, usually 1.1 x gauge set pressure, bara or psia
- M : molecular weight
- z : compressibility factor
- $T(*)$: vapor temperature, °K or °R
- $\rho_L(*)$: liquid density, kg/m³ or lb/ft³

4. Relief Load Result

Standard	API-521	Topsoe	TCC
Wg	21675 kg/h	19680 kg/h	20309 kg/h



5. Use the formula below to calculate orifice area

Gas or Vapor Relief – Critical flow

In USC units:

$$A = \frac{W}{CK_d P_1 K_b K_c} \sqrt{\frac{TZ}{M}}$$

$$A = \frac{V \sqrt{TZM}}{6.32 CK_d P_1 K_b K_c}$$

$$A = \frac{V \sqrt{TZG_v}}{1.175 CK_d P_1 K_b K_c}$$

In SI units:

$$A = \frac{W}{CK_d P_1 K_b K_c} \sqrt{\frac{TZ}{M}}$$

$$A = \frac{2.676 \times V \sqrt{TZM}}{CK_d P_1 K_b K_c}$$

$$A = \frac{14.41 \times V \sqrt{TZG_v}}{CK_d P_1 K_b K_c}$$

USC:

$$C = 520 \sqrt{k \left(\frac{2}{k+1} \right)^{\frac{k+1}{k-1}}}$$

SI :

$$C = 0.03948 \sqrt{k \left(\frac{2}{k+1} \right)^{\frac{k+1}{k-1}}}$$

P_1 is the upstream relieving pressure, psia (kPa); this is the set pressure plus the allowable overpressure

K_b is the capacity correction factor due to backpressure

K_c is the combination correction factor for installations with a rupture disk upstream of the PRV equals 1.0 when a rupture disk is not installed. K_c equals 0.9 when a rupture disk is installed in combination with a PRV and the combination does not have a certified value.

T is the relieving temperature of the inlet gas or vapor, °R (°F + 460) [K (°C + 273)]

Z is the compressibility factor for the deviation of the actual gas from a perfect gas, a ratio evaluated at inlet

6. Results

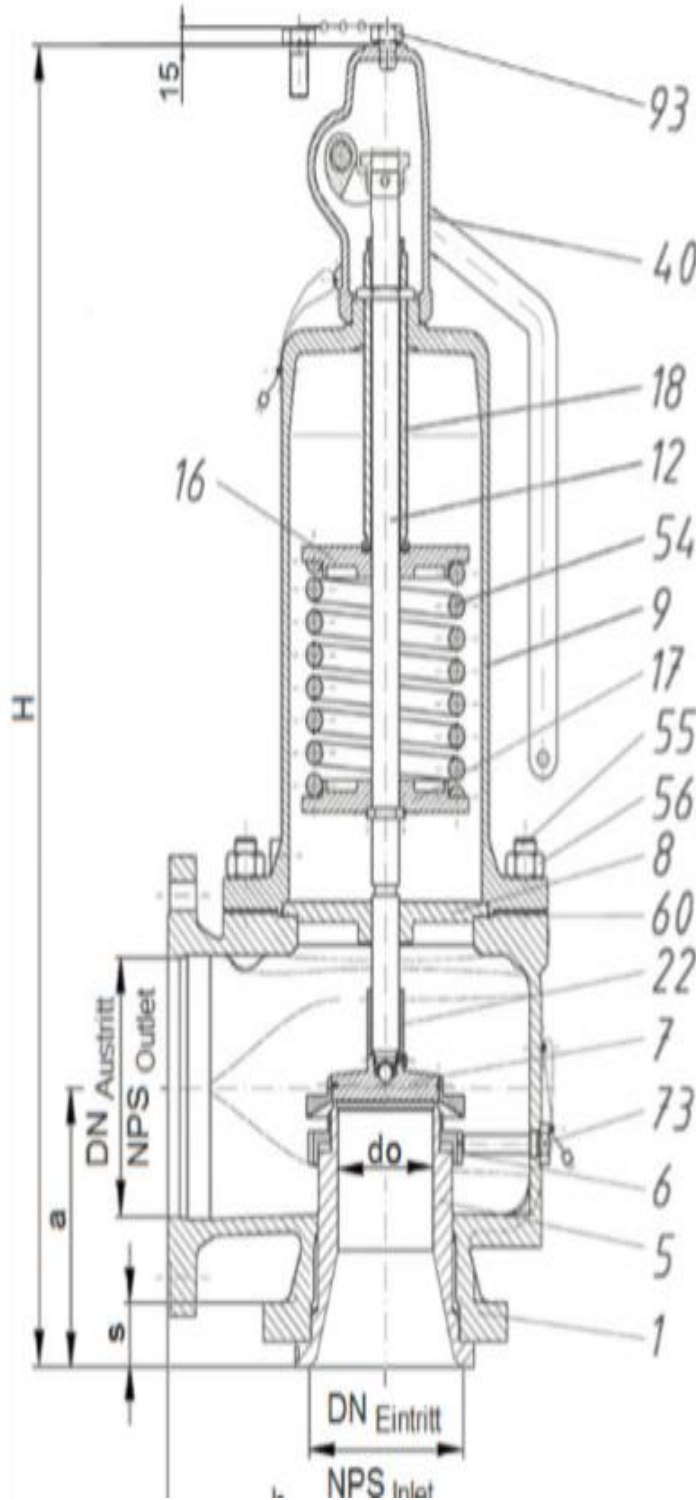
Standard	API-521	Topsoe	TCC
Orifice area	50 cm2	45.28 cm2	



Table 14—Spring-loaded Pressure-relief Valves “Q” Orifice ^f (Effective Area = 11.05 in.²)

Materials ^b	Valve Size	ASME Flange Class		Maximum Inlet Flange (Set) Pressure Limit ^a (psig)						Outlet Pressure Limit ^a (psig)		Center-to-Face Dimensions (in.)	
		INLET	OUTLET	Conventional and Balanced Bellows Valves						Flange Rating Limit ^a	Bellows Rating Limit ^a	INLET	OUTLET
-450 °F to -76 °F	-75 °F to -21 °F			-20 °F to 100 °F	450 °F	800 °F	1000 °F	100 °F	100 °F				
Temperature Range Inclusive -20 °F to 800 °F													
Carbon Steel	6Q8	150	150			(165)	(165)	80		(115)	70	9 7/16	9 1/2
	6Q8 ^c	300	150			(165)	(165)	(165)		(115)	70	9 7/16	9 1/2
	6Q8	300	150			(300)	(300)	(300)		(115)	115	9 7/16	9 1/2
	6Q8	600	150			(600)	(600)	(600)		(115)	115	9 7/16	9 1/2
Temperature Range Inclusive 801 °F to 1000 °F													
Chrome Molybdenum Steel	6Q8	300	150					(165)	(165)	(115)	115	9 7/16	9 1/2
	6Q8	600	150					(600)	430	(115)	115	9 7/16	9 1/2
Temperature Range Inclusive -450 °F to 1000 °F													
Austenitic Stainless Steel	6Q8	150	150	(165)	(165)	(165)	(165)	80	20	(115)	70	9 7/16	9 1/2
	6Q8 ^c	300	150	(165)	(165)	(165)	(165)	(165)	(165)	(115)	70	9 7/16	9 1/2
	6Q8	300	150	(250)	(300)	(300)	(300)	(300)	(300)	(115)	115	9 7/16	9 1/2
	6Q8	600	150	(300)	(600)	(600)	(600)	(600)	(600)	(115)	115	9 7/16	9 1/2

According to table above 6Q8 is selected. Due to low Pb/Pset conventional type can be selected



Specific Valve Data		
Pos	Description	Data
1	Purchase Order No.	A-2-1CN22101-Methanol/HK170434es-1
2	LESER Job No.	20329048
3	LESER Pos.	160
4	Type	5202.6584
5	Orifice	Q
6	Inlet size	NPS 6"
7	Inlet pressure rating	300 lbs ASME B16.5
8	Inlet flange facing	Serr spiral finish, Ra=3,2-6,3
9	Outlet size	NPS 8"
10	Outlet pressure rating	150 lbs ASME B16.5
11	Outlet flange facing	Serr spiral finish, Ra=3,2-6,3
12	d0 [mm]	105,50
13	Set pressure	7,50
14	Pressure unit	bar-g
15	CDTP [bar-g]	7,50
16	Dimension a [mm]	240,00
17	Dimension b [mm]	243,00
18	Dimension s [mm]	57,00
19	Dimension H [mm]	1056,00
20	Weight [kg]	223,00
21	Tag No. 1 + 2	PSV-3143; PSV-3146
22	Tag No. 3 + 4	PSV-3149
23	Tag No. 5 + 6	
24	Tag No. 7 + 8	
25	Tag No. 9 + 10	
26	Tag No. 11 + 12	

List of Parts Main Valve			
Pos	Description	Qty	Material
1	Body	1	1.0619 / WCB / WCC
5	Nozzle	1	1.4408 / CF8M (stainless)
6	Adjusting ring	1	1.4408 / CF8M
7	Disc AS	1	1.4401 / 1.4404 / 316 / 316L (stainless)
8	Guide AS	1	1.0460 / SA-105
9	Bonnet	1	1.0619 / WCB / WCC
12	Spindle	1	1.4021 / Chrome Steel
16	Spring Plate	1	1.0460 / SA-105
17	Spring Plate	1	1.0460 / SA-105
18	Adjusting Screw AS	1	1.4104 / 430F + PTFE / Glas
22	Lift stopper	1	1.4401 / 1.4404 / 316 / 316L
40	Cap / Lifting Device AS	1	10.7040 / 60-80-18
54	Compression Spring	1	1.8109 (SAE) or 1.7110 (SAE) or F640 / High temp. Alloy Steel
55	Stud	12	1.4401 / Stainless Steel
56	Hexagon Nut	12	1.4401 / Stainless Steel
60	Gasket	1	Graphite / 3.4401 / Stainless Steel
73	Lock screw	1	1.4401 / 1.4404 / 316 / 316L
93	Test Gag AS	1	1.4401 / Stainless Steel